

REINHOLD ENVIRONMENTAL Ltd.



2011 NO_x-Combustion Round Table & Expo Presentation

February 7-8, 2011, in Birmingham, AL / Hosted by Southern Company

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**Reinhold Environmental LTD.
2011 NOx-Combustion / PCUG Conference**

SCR Catalyst Regeneration

February 7, 2011



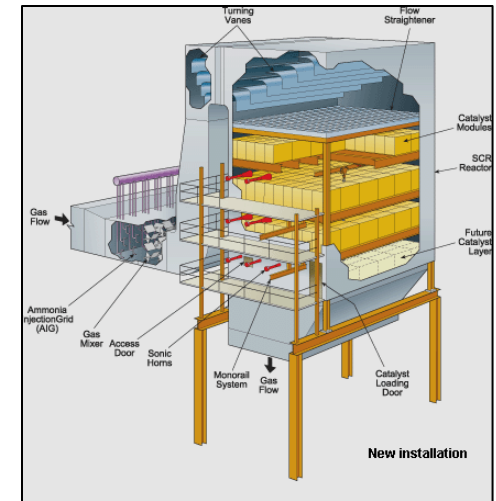
**Michael F. Mattes
Chief Operating Officer**

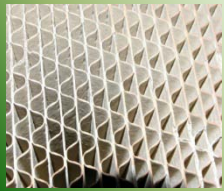
Agenda

Meeting the World Energy Challenge.

CoaLogix™

- **Anatomy of SCR Catalyst**
- **Common Catalyst Processing Terms**
- **Deactivation Mechanisms**
- **How Regeneration Work?**
- **Regenerated Catalyst Performance**
- **Operating Experience with Regenerated Catalyst**
- **Factors to Consider When Purchasing SCR Catalyst**



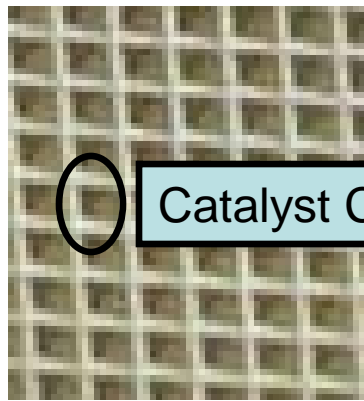


Anatomy of SCR Catalyst



Reaction Zones

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Catalyst Cell



Diffusion Controlled
DeNO_x and Hg
Region
0 to ~0.2 mm

Catalyst
Pore

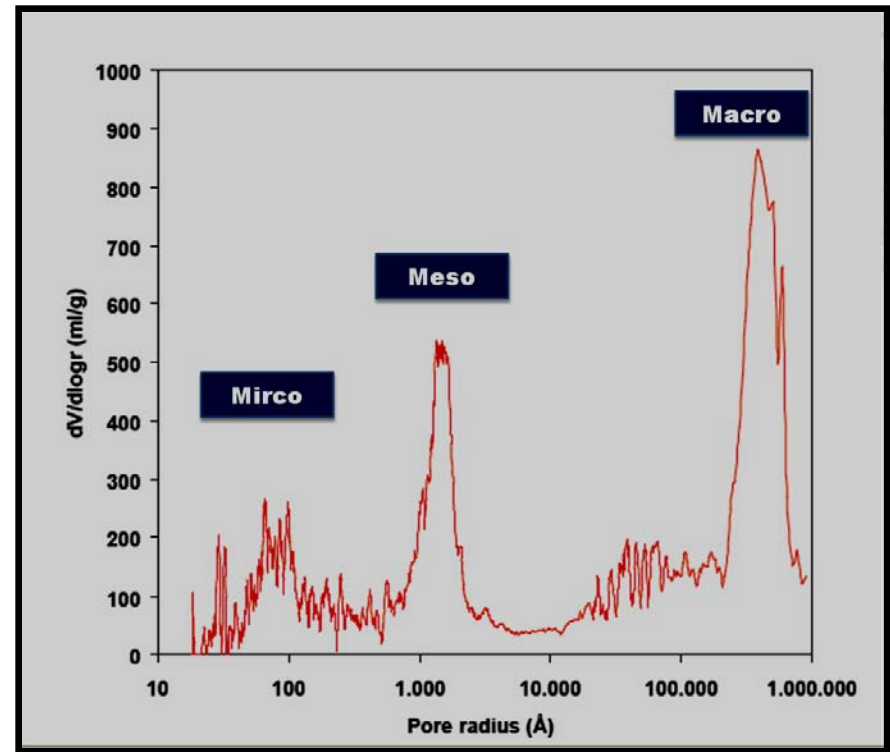
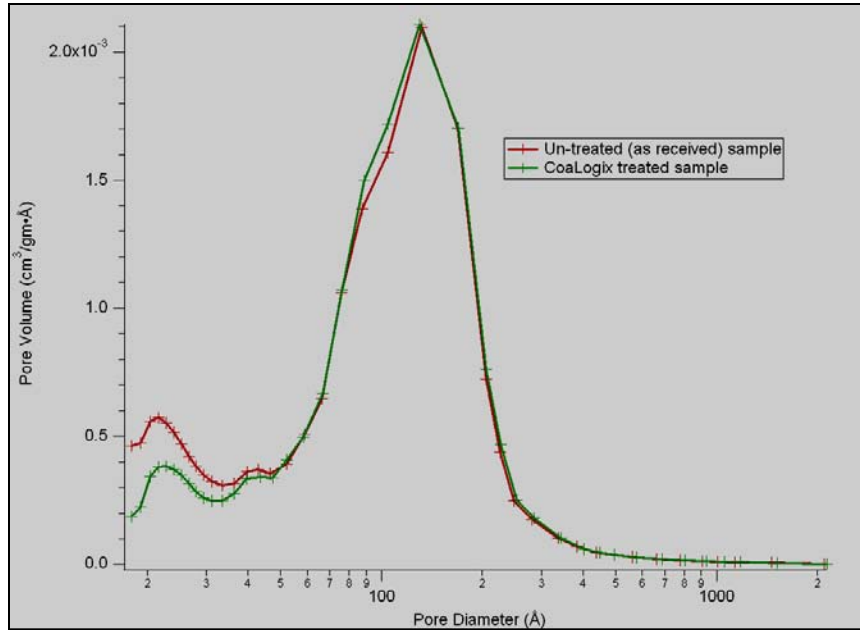
Honeycomb
Element

Kinetically Controlled
SO₂ Oxidation Region
~0.2 - 1.0 mm.
"Low NH₃"

Flue Gas Residence Time ~ 0.15 seconds per Layer

Pore Size - Angstroms

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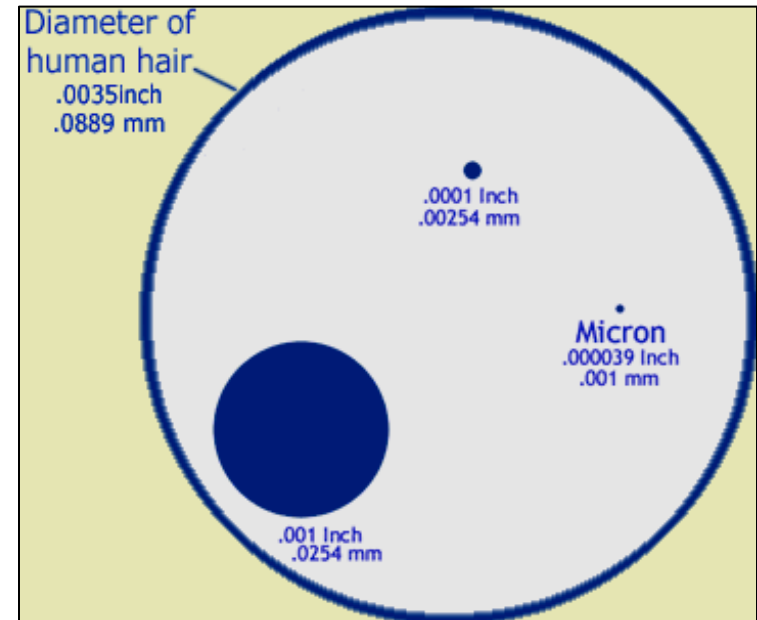


Varies by Manufacturer

Pore Sizes

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Pore Classification		Pore Size	
		Angstroms	Microns
Micro	Smallest	30	0.003
Meso	Medium	500	0.05
Macro	Largest	1,000	0.1
NO _x Molecule		8	0.0008



Human Hair ~ 900,000 Angstroms

Catalyst Surface Area

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Catalyst Surface Area

Catalytic Surface Area	65	Sq. Meters / Gram
Visible Specific Area	480	Sq. Meters / Cubic Meter



Catalyst Surface Area



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Catalyst Surface Area				
	Metric Units		English Units	
Catalytic Surface Area	65	Sq. Meters / Gram	19,845	Sq. Feet / Ounce
Visible Specific Area	480	Sq. Meters / Cubic Meter	45	Sq. Feet / Cubic Feet
Catalyst Volume	2.10	Cubic Meters / Module	74.2	Cubic Feet / Module
Catalyst Weight	680	Kilograms / Module	1,500	Lbs / Module
Visible Surface Area	1,008	Square Meters / Module	10,846	Sq. Feet / Module
Catalytic Surface Area	44,226,000	Sq. Meters / Module	476,291,400	Sq. Feet / Module
Ratio Catalytic to Visible Surface Area			~44,000 to 1	

650 Mw Unit has ~ 10,000 Sq. Miles of Catalytic Surface Area

10,000 Square Miles

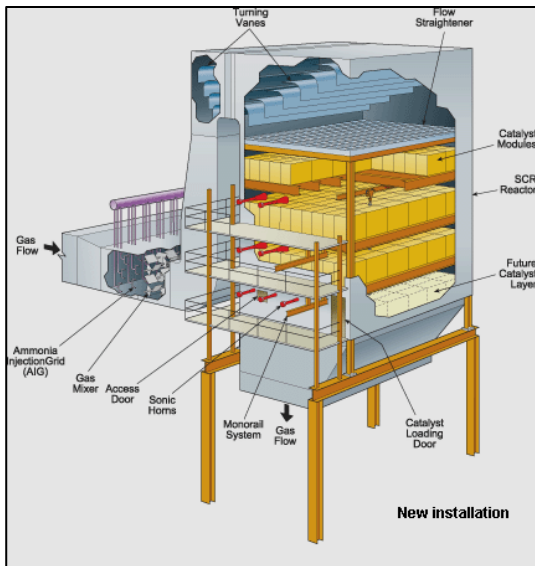
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OEM Magic of Calcination

Common Catalyst Processing Terms



Common Terms

Term	Definition
Dry Mechanical Cleaning	Utilizes compressed air and vacuum to removed loose fly ash.
Rejuvenation	Wet process to primarily remove “physical “ pluggage. No addition of active ingredient(s).
Regeneration	Wet process to remove desired compounds (decay chemicals and/or active ingredients). Followed by re-impregnation of active ingredient(s) .
Re-impregnation	Addition of active ingredient(s). May be one or more ingredients applied separately or simultaneously.
Drying	Removes free water. Normally at temperatures < 250 ° F.
Heat Treatment	Removes the required bound water and properly activates the added active ingredient(s). Temperature varies by regeneration process used.
Calcination	One time event performed by catalyst OEM’s to produce its “catalytic” surface area, strength and performance properties.

Temperature Zones

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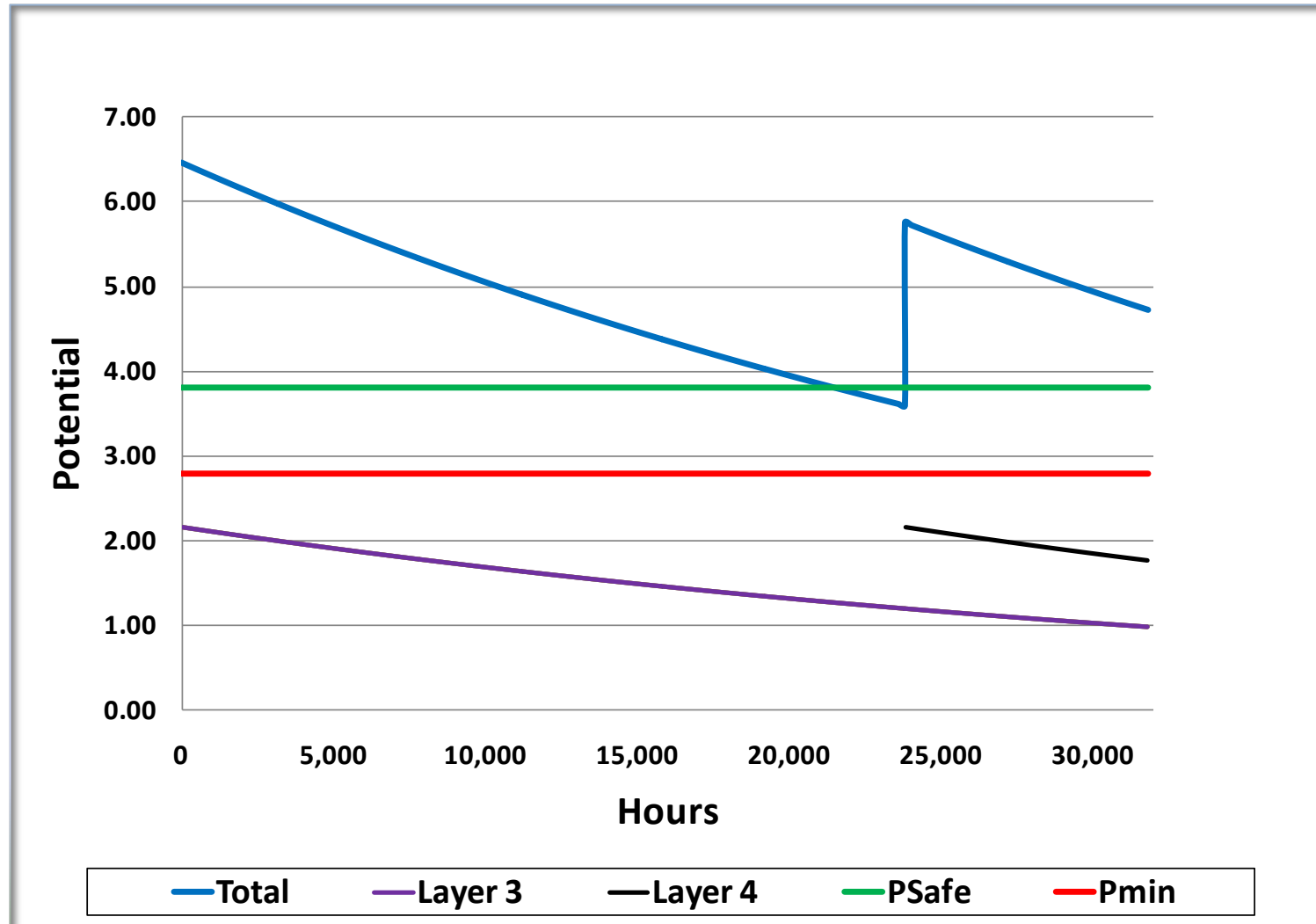
Avoid OEM Calcination Temperatures

Common Terms

Term	Symbol	Units	Definition
DeNOx Activity	K	m/hr	$K = P \cdot AV$ Analogy - Speed of a car
Area Velocity	AV	m/hr	$AV = \text{Flue Gas Flow} / \text{Visible Catalyst Surface Area}$ Analogy - Inverse of residence time
Potential	P	Unitless	$P = -\ln(\text{Fraction Nox Remaining})$ Analogy - Distance a car can travel Very useful tool in catalyst management Potential being a log function is additive Key to predicting SCR performance over time

Typical SCR Decay Curve

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Area Velocity

$$\begin{array}{l} \textit{Area Velocity (AV)} \\ (m/hr) \end{array} = \begin{array}{l} \textit{Flue Gas Flow} \\ (Nm^3 / hr) \end{array} \div \begin{array}{l} \textit{Catalyst Visible Surface Area} \\ (m^2) \end{array}$$

$$\begin{array}{l} K \\ (m/hr) \end{array} = \begin{array}{l} P \\ (unitless) \end{array} * \begin{array}{l} AV \\ (m/hr) \end{array}$$

Area Velocity High – Residence Time in Catalyst Low

$$\textit{Potential} = -\ln \left[1 - \frac{NOx_{in} - NOx_{out}}{NOx_{in}} \right]$$

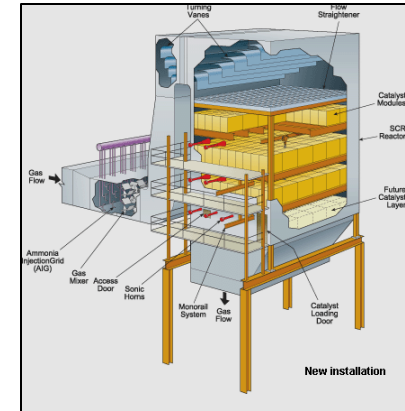
$$\textit{Potential} = -\ln \left[1 - \frac{\textit{Fraction NOx Removed}}{NOx_{in}} \right]$$

$$\textit{Potential} = -\ln \left[\frac{\textit{Fraction NOx Remaining}}{NOx_{in}} \right]$$

Example Calculations

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	Value	Units
Visible Surface Area	1,000	M ² / Module
Modules	192	Per Layer
Visible Surface Area	192,000	M ² / Layer
Flue Gas Flow	2,880,000	Nm ³ / hr
Area Velocity (AV)	12.0	m / hr

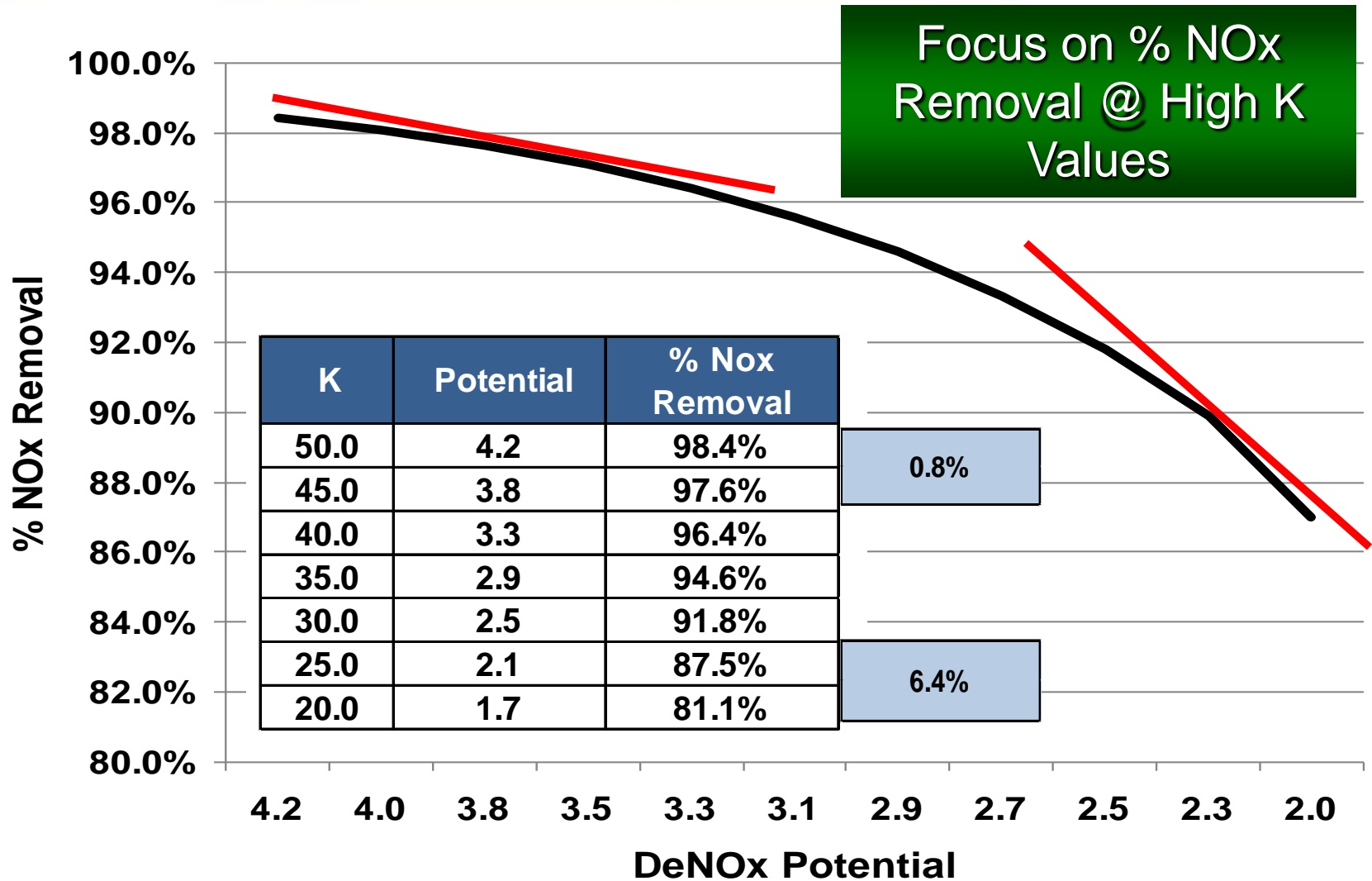


Measured		Calculated			
NOx _{in}	NOx _{out}	NOx Remaining	NOx Removed	Potential = -ln (Nox Remaining)	K = P * AV
ppmvd	ppmvd	Fraction	%	Unitless	m / hr
500	150	0.30	70%	1.20	14.4
500	100	0.20	80%	1.61	19.3
500	50	0.10	90%	2.30	27.6
500	25	0.05	95%	3.00	35.9
500	15	0.03	97%	3.51	42.1

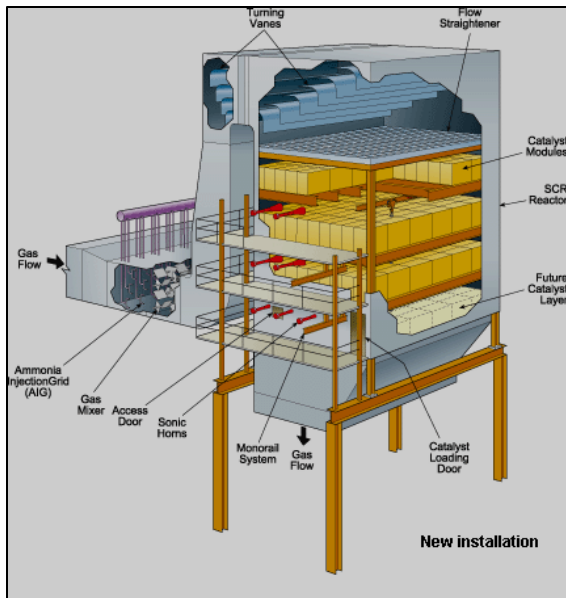
Potential is a Better Measure of Catalyst Performance

Potential Vs % NOx Removal

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Deactivation Mechanisms



Positive Reactions:

No_x Reduction



Hg Oxidation



Negative Reactions:

SO₂ Oxidation



HgCl₂ Reduction by NH₃



HgCl₂ Reduction by SO₃



SCR Challenges



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	Parts per Million			Parts per Billion			Ratio to Hg ²⁺ Concentration		
	Inlet SCR	Exit SCR	FGD Outlet	Inlet SCR	Exit SCR	FGD Outlet	Inlet SCR	Exit SCR	FGD Outlet
SO ₂	2,500	2,475	124	2,500,000	2,475,000	123,750	1,250,000	412,500	1,237,500
SO ₃	25	50	30	25,000	50,000	30,000	12,500	8,333	300,000
NO _x	500	75	75	500,000	75,000	75,000	250,000	12,500	750,000
Hg ⁰	0.08	0.02	0.03	8	2	3	4	0	30
Hg ²⁺	0.02	0.06	0.00	2	6	0.1	1	1	1
Hg Total	0.10	0.08	0.03	10	8	3	5	1	31

SCR's Performing Beyond Original Design

SCR Vs Catalyst Performance

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		Primarily Affected By	
SCR Performance	Catalyst Performance	Catalyst Decay Rate	Flue Gas Impurities
			Operating Conditions
		Temperature	
		Flue Gas Velocity	
		SO ₃ Concentration - 0 to 10ppm	
		NH ₃ Concentration < 1.0 Mole Ratio	
	% Catalyst Pluggage		
	% Flue Gas By-pass		

➤ Thermal sintering

- Excessive temperature > 900 ° F
- Leads to loss in catalytic surface area
- Not common in coal fired units

➤ Mechanical erosion

- < 30% pluggage - Minor
- > 30% to 50% pluggage - Significant
- >50% pluggage – Very Severe

Irreversible

➤ Catalyst plugging

- Fly ash near inlet wall
- LPA / “popcorn ash”
- **Often the controlling decay mechanism**
- Easily detected

➤ Pore mouth blinding

- Silica & aluminum-silicate
- CaSO_4
- CaCO_3
- A common form of activity loss

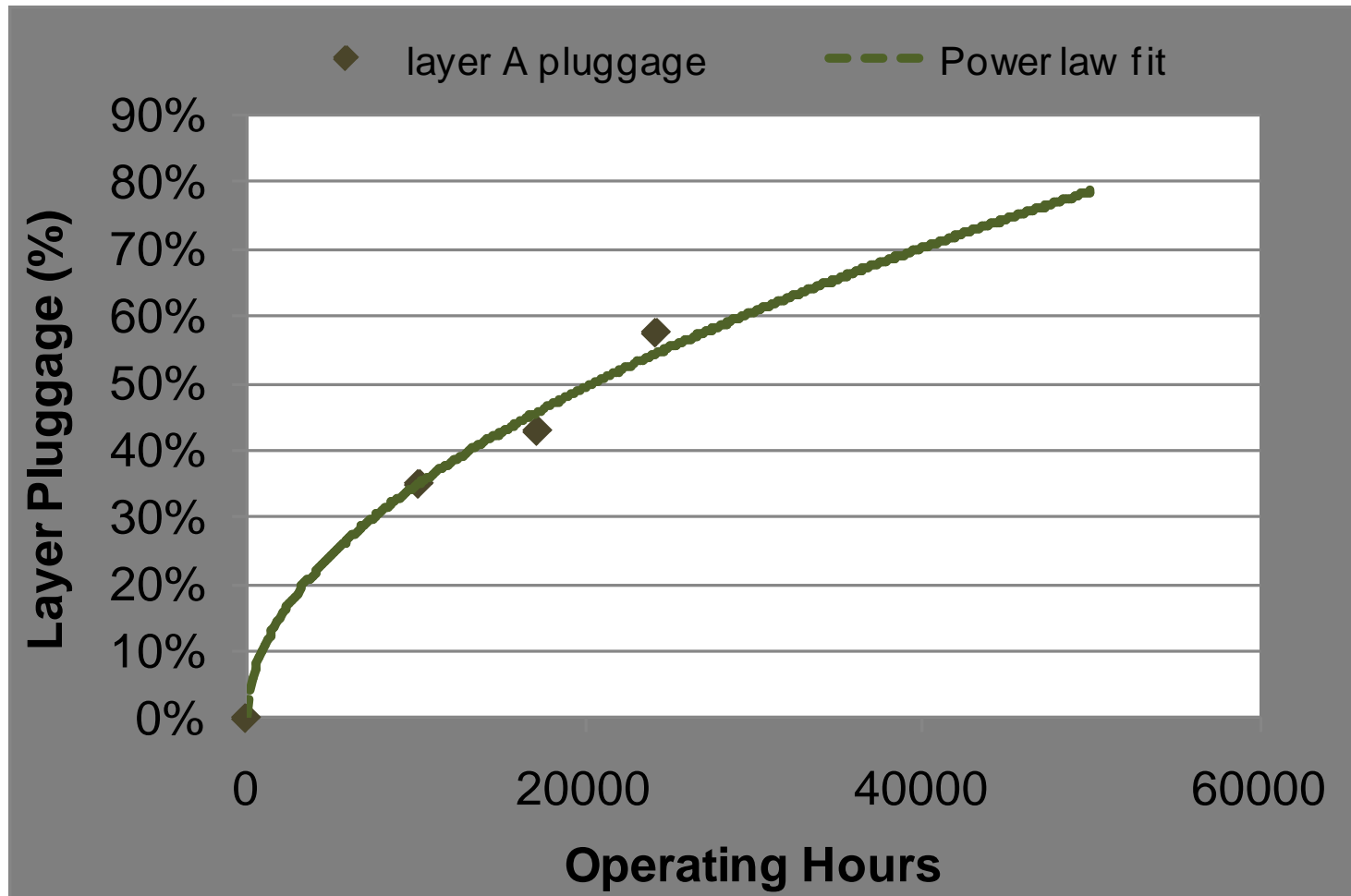
Reversible

- Alkaline metal (Na, K)
- Phosphorous
 - High phosphorous coals fired in "reducing environment" (low NOx burners) generated PX_3 species that actively poison V_2O_5 V-P complex
- Arsenic – 2 mechanisms
 - Gaseous arsenic (As_2O_3) condenses in catalyst pore
 - Further oxidation to solid As_2O_5 to permanently plugs pore mouth
 - Combines with vanadium to form inactive V-As species

Reversible

SCR Catalyst Pluggage

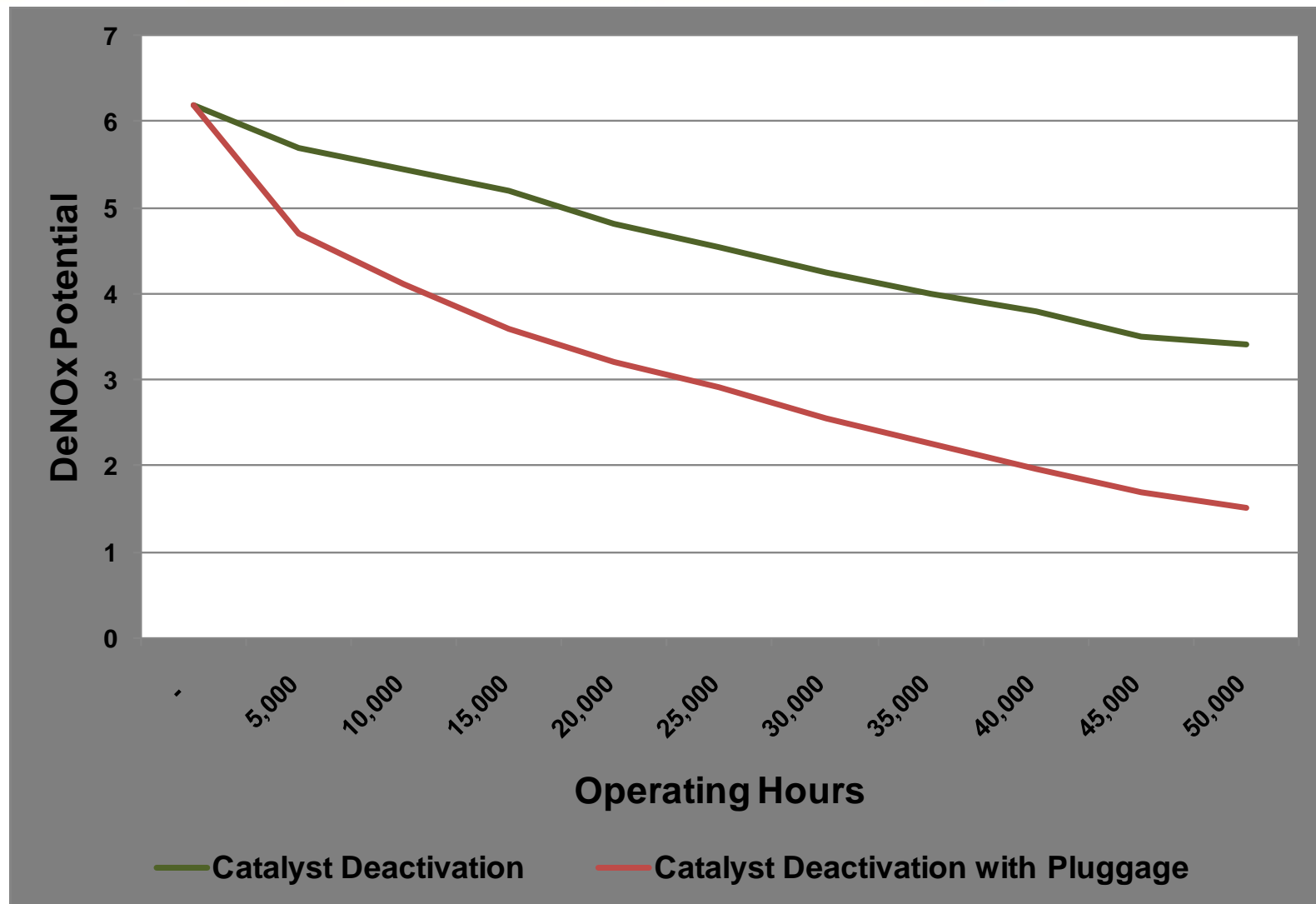
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Pluggage – Increases erosion

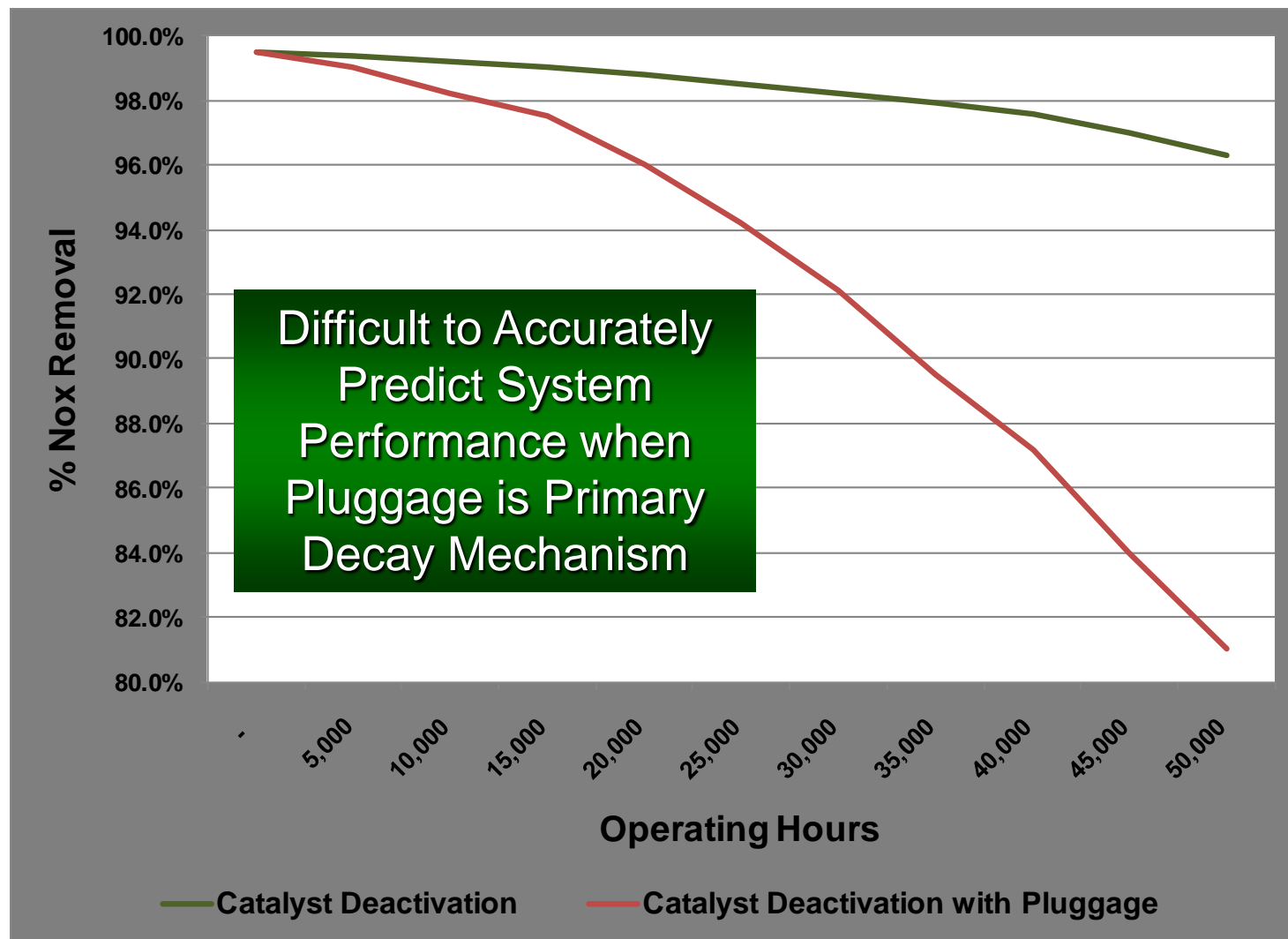
Affect of SCR Pluggage

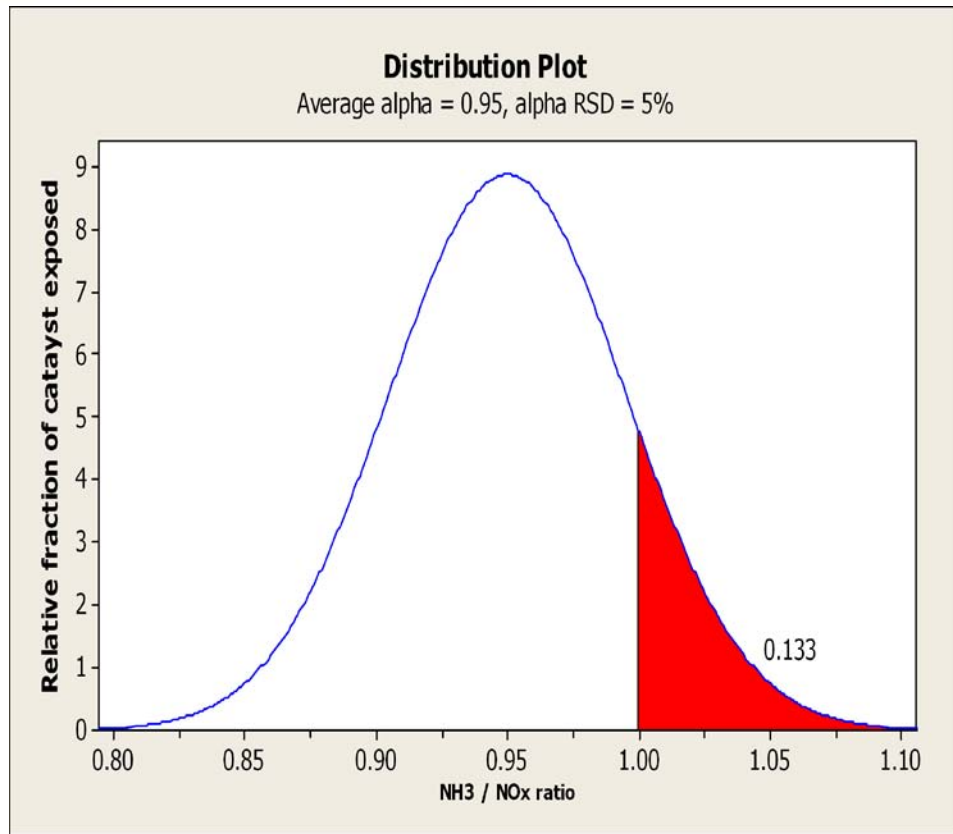
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Affect of SCR Pluggage

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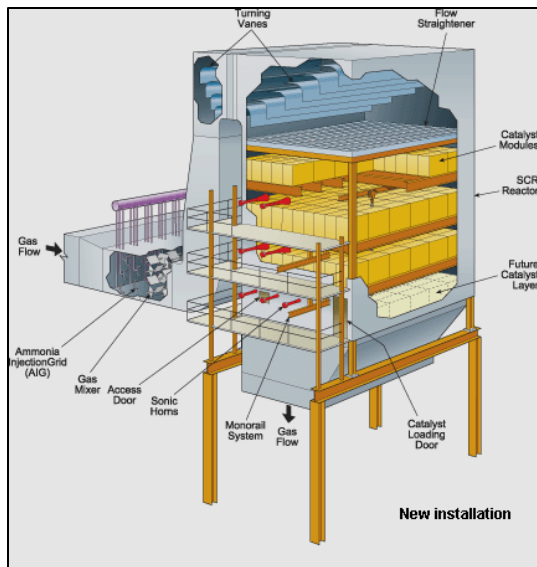


% NH ₃ Imbalance	Actual % Nox Removal
0%	90%
5%	90%
10%	88%
15%	86%
20%	83%
25%	81%
30%	78%
35%	76%
Base Efficiency	95%
NH ₃ Flow at 0.95 molar ratio	

Normal Range

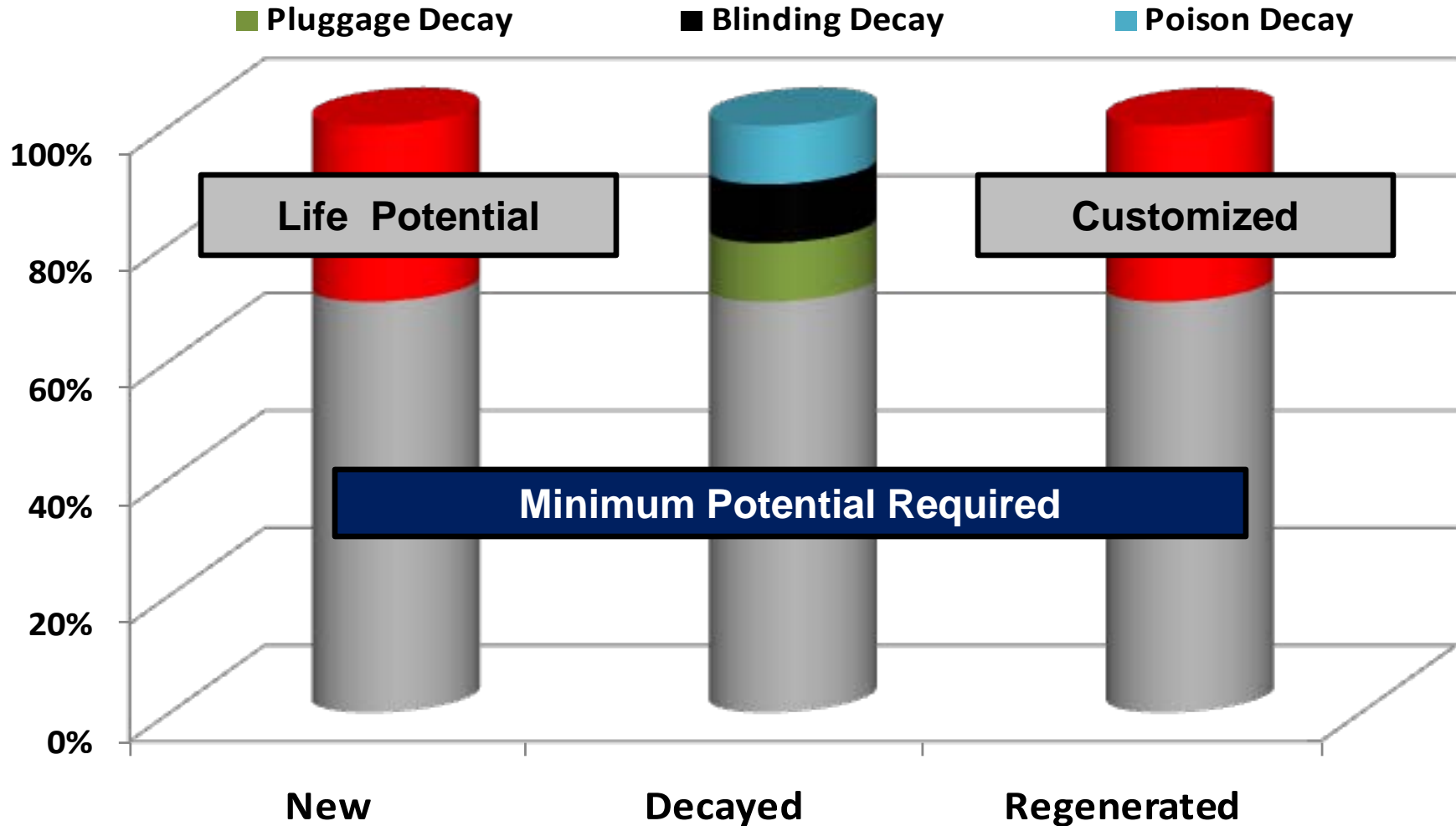
NH₃ Imbalance Affects DeNO_x and NH₃ Slip

How Does Regeneration Work?



How Does Regeneration Work?

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Regeneration Process

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**Dry Mechanical
Cleaning**

Plate catalyst disassembled.
Can hold > 2,000 lbs. of fly ash

**Wet Chemical
Treatment**

Precise control, mild chemicals, removes remaining
physical pluggage

Ultrasonic Treatment

Utilized as required. Allows removal of difficult
contaminants with mild chemicals.

Pre-Drying

Removal of all cleaning compounds and impurities.
Critical to catalyst performance. Especially SO₂
conversion.

Drying

Removal of free water. Amount varies by catalyst
type and size. Can be > 100 gallons per module.



Regeneration Process

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Drying

Continuation

Re-impregnation

Customized to meet requested performance. Primarily places chemicals in the DeNO_x and Hg oxidation vs. SO₂ Conversion zone.

Final Heat Treatment

Removes bound water, properly activates the added ingredient(s) and strengthens catalyst. Temperature varies by regeneration process used.

Repairs

Module casings and catalyst elements or cassettes.

Storage

Weather controlled. Capacity for > 12,000 modules.



Process Results

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Corrugated

Honeycomb

Plate



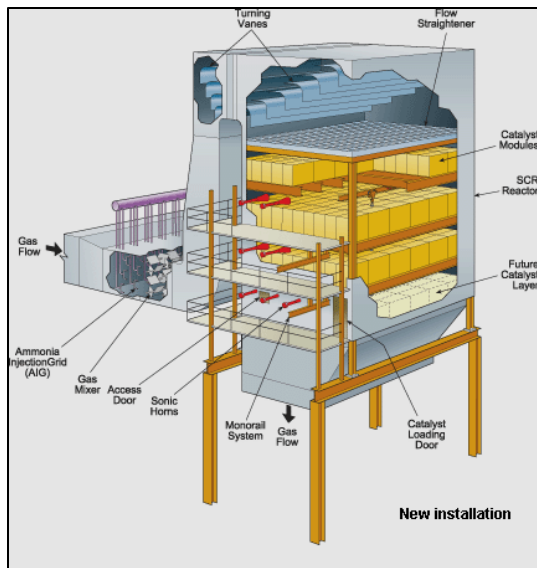
Before



After

Proven with all catalyst types since 1998

Regenerated Catalyst Performance



- **Performance equal to the original catalyst**
 - DeNO_x Potential
 - SO₂ conversion
 - Hg oxidation – Need more data!
 - Pressure drop - % pluggage < 5% per layer

- **Customized Performance**
 - Adjust active ingredient(s) for proposed operating conditions
 - Can normally improve performance by placing active ingredient(s) in preferred reaction zone.

Re-impregnate catalyst based on where it is going

- **Crush tests have significant variances**
 - Sensitive to micro cracks
 - More important to guarantee condition of catalyst returned to customer

- **Erosion tests more useful**
 - Method very important
 - Good relative test

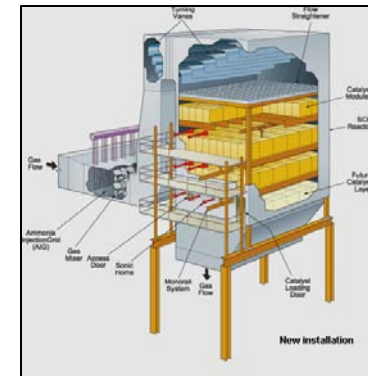
°F	Ratio of Mass Removed			Average	Std. Dev.
	1	2	3		
400	0.89	1.07	0.93	0.96	0.09
600	0.92	0.83	0.98	0.91	0.08
800	1.07	1.02	0.87	0.99	0.10

Ratio is to a new control sample tested at the same time.

What to Expect?

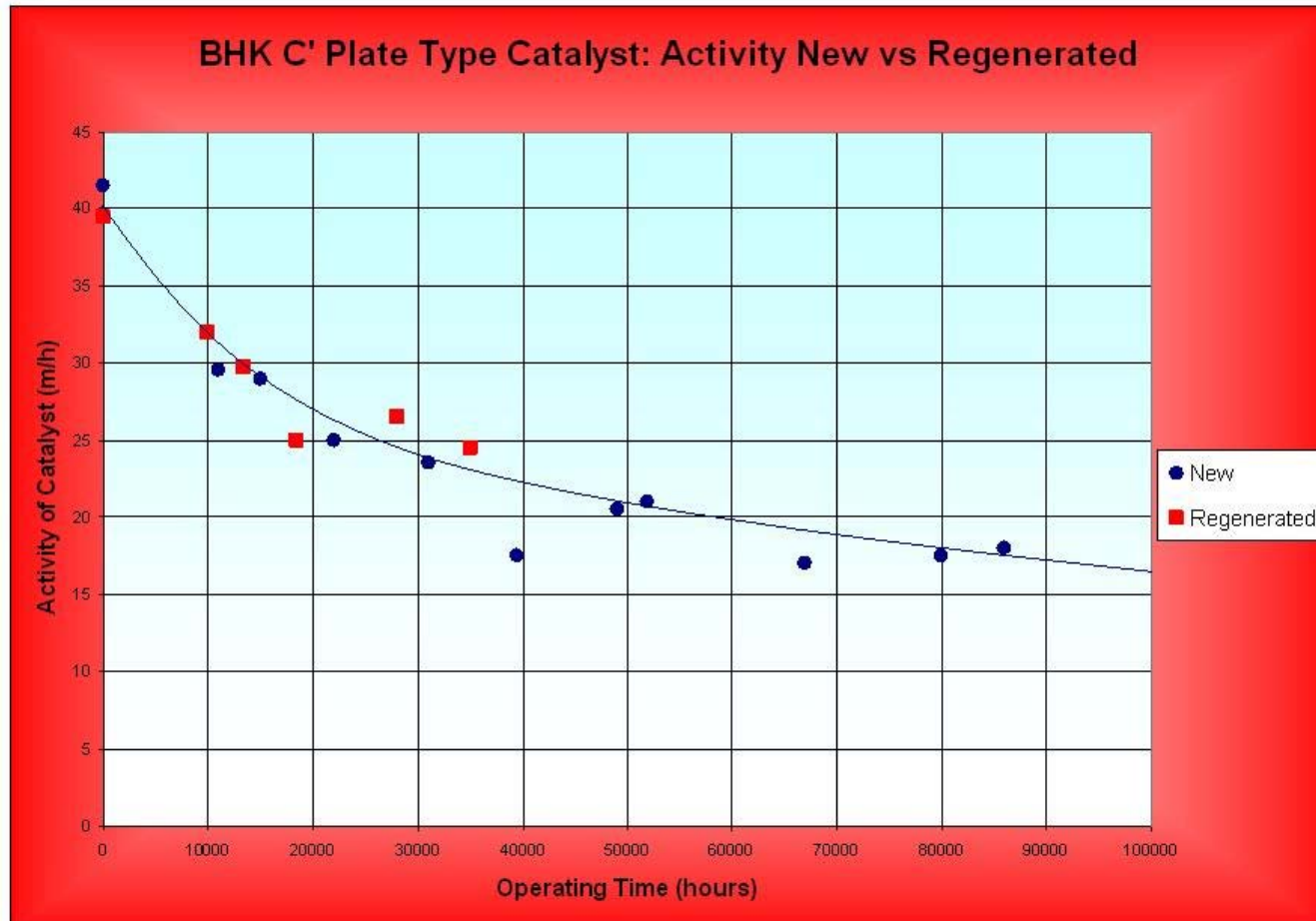
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- Same decay rates as original catalyst
- Testing capability
- **Hot Regeneration** - Ability to regenerate catalyst during your outage
- Brokering of catalyst
- Assist in disposal options
- Catalyst availability – Weeks with NOxAssure
- Storage



Decay Rates vs. New

long-term deactivation



How Many Times for Regeneration?

- **Depends on:**
 - % pluggage
 - Exposure to moisture
 - Handling - removal and installation
 - Location in SCR

- **Ability to regenerate can be determine with annual inspections**

- **Bottom cassette layers will likely last longer**

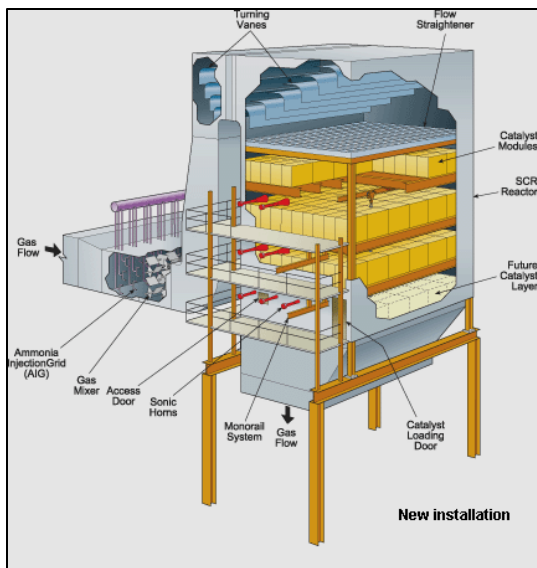
Normally Assume 3 Regenerations for Budgets

Variations in Regeneration

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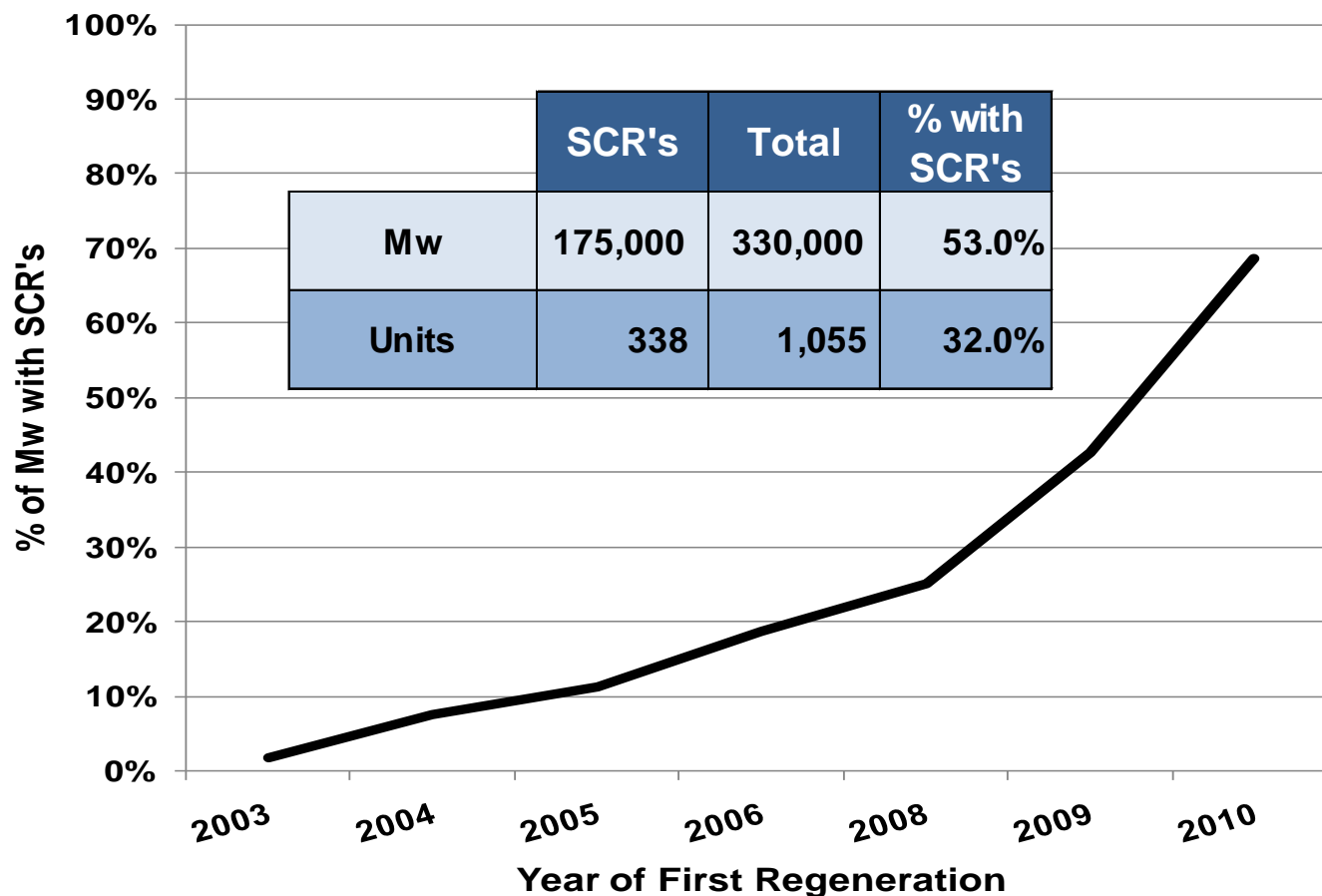
	Significance	Comments
Original Manufacturing	Low	OEM's have good AC/QC procedures
Exposure to Flue Gas	Low to High	% and rate of pluggage
Exposure to Moisture	Low to High	Air and tube leaks
		Shutdown and storage procedures
		Especially important for plate catalyst where "rusted iron" can be an issue for SO ₂ conversion
Catalyst Testing	Medium to High	Full bench vs. micro
		Extrapolation from standard operating conditions
		Stability of catalyst
		Inlet SO ₃ concentration - Can be very significant
		Molar ratio NH ₃ to NO _x
		Sampling method, etc.

Operating Experience with Regenerated Catalyst



Regeneration Market Share

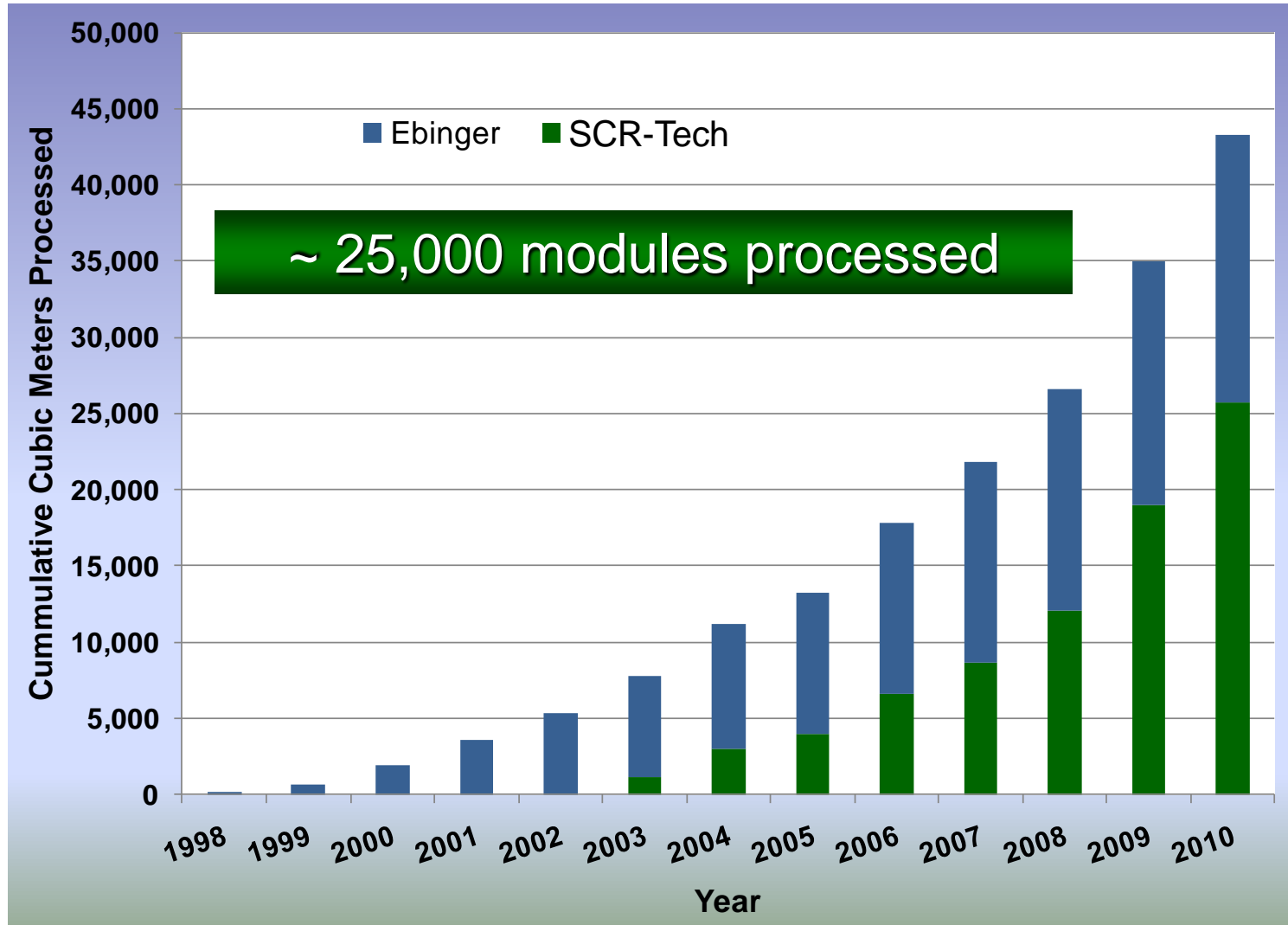
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70% of the Utilities with SCR's have Regenerated Catalyst

SCR-Tech Experience

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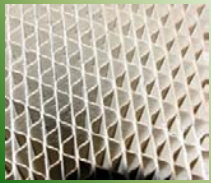
SCR-Tech Experience

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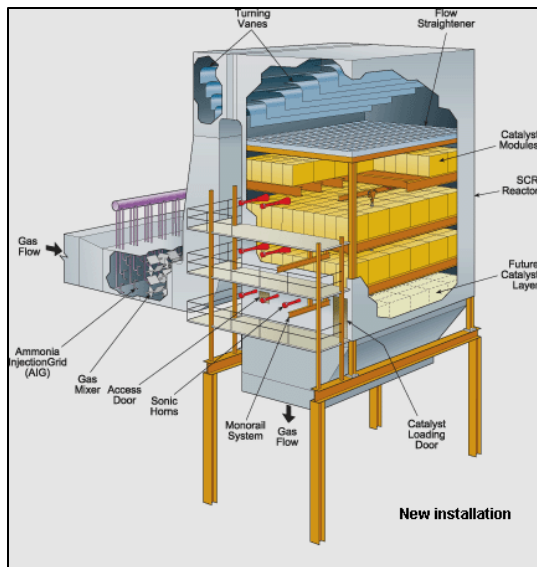
Corrugated
15%

Plate
30%

Honeycomb
55%



Factors to Consider When Purchasing SCR Catalyst



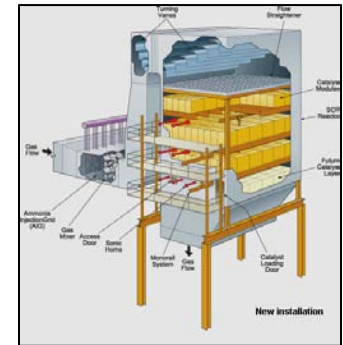
Factors to Consider

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Item	Comments
Pitch	Number one item
	Insure that pluggage will be <15%
Screen Size	Normally slightly smaller then "free opening" (pitch - wall thickness) of catalyst
	Screen pluggage can lead to catalyst erosion
Value	\$ / potential, not \$ per layer or \$ / cubic meter
	Balance of performance - DeNOx, SO2 conversion, Hg oxidation, pressure drop, life
	Support, experience and technical expertise
Plate Catalyst	Know the quality of the mesh - 400 vs. 300 series stainless steel
	Can lead to future SO2 conversion issues

- **Regeneration is a proven technology**
- **Should be part of your overall catalyst management strategy**
- **Customized regeneration available to assist in catalyst management flexibility**
- **Brokering (selling or purchasing) previously owned catalyst may be a helpful option**
- **Regenerated catalyst can be available in weeks**



**Reinhold Environmental LTD.
2011 NOx-Combustion / PCUG Conference**

Thank-you

February 7, 2011



**Michael F. Mattes
Chief Operating Officer**